Further Results on Robust Output Feedback Control for the Chemostat Dynamics

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Figure 1: Chemostat



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Bioreactor.



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Bioreactor. Fresh medium continuously added.



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Bioreactor. Fresh medium continuously added. Culture liquid continuously removed.



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Bioreactor. Fresh medium continuously added. Culture liquid continuously removed. Culture volume constant.

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$$\begin{split} & \mathcal{K}_{0} = \\ & \min\left\{\frac{\mu_{1}(s_{\text{in}}) - \mu_{1}(s_{*})}{(a+1)x_{1*} + 2ax_{2*}}, \frac{\mu_{1}(s_{*})}{4(a+1)s_{\text{in}}}, \frac{1}{a}\min\left\{\mu_{i}'(s) : s \in [0, s_{\text{in}}], i = 1, 2\right\}\right\} \\ & \text{Let } \sigma : \mathbb{R} \to [-1, 1] \text{ denote the usual saturation.} \end{split}$$

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Theorem: For each constant $K \in (0, K_0)$ and each constant a > 1, (NV) in closed loop with the bounded positive controller

$$D(y) = \mu_1(s_*) - 2(1+a)s_{in}K\sigma\Big(\frac{1}{2(1+a)s_{in}}[y - x_{1*} - ax_{2*}]\Big)$$
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Proof: Use Poincaré-Bendixson Theorem and dimension reduction.

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Corollary: We can choose K and a constant $\varepsilon > 0$ such that if $\mathcal{T}(\mu, \nu) = \max\{|\mu_i'(s) - \nu_i'(s)| : i = 1, 2; s \in [0, s_{in}]\} < \varepsilon$, then $\begin{cases}
\dot{s} = D(y)[s_{in} - s] - \nu_1(s)x_1 - \nu_2(s)x_2 \\
\dot{x}_i = [\nu_i(s) - D(y)]x_i, i = 1, 2
\end{cases}$ (RC)

is GAS to some point $(s_{\nu}, x_{1\nu}, x_{2\nu}) \in (0, \infty)^3$.

$$\begin{cases} \dot{s} = (s_{in} - s)D(y) - \frac{0.05sx_1}{20 + d_1 + s} - \frac{0.052sx_2}{25 + d_2 + s}, \\ \dot{x}_1 = \left[\frac{0.05s}{20 + d_1 + s} - D(y)\right]x_1, \\ \dot{x}_2 = \left[\frac{0.052s}{25 + d_2 + s} - D(y)\right]x_2 \\ y = x_1 + 1.2x_2 \end{cases}$$
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$$D(y) = 0.042 - 0.00924616\sigma\left(\frac{y - 0.074}{462.308}\right)$$
(C)







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- Unlike the standard GAS treatments, our output feedback is a decreasing function of the output.
- Desirable extensions would allow nonmonotone µ_i's, more than two species, or multiple limiting substrates.