

Recent Results on Control Problems for Chemostats

Michael Malisoff, Louisiana State University

Joint work with Frédéric Mazenc from INRIA

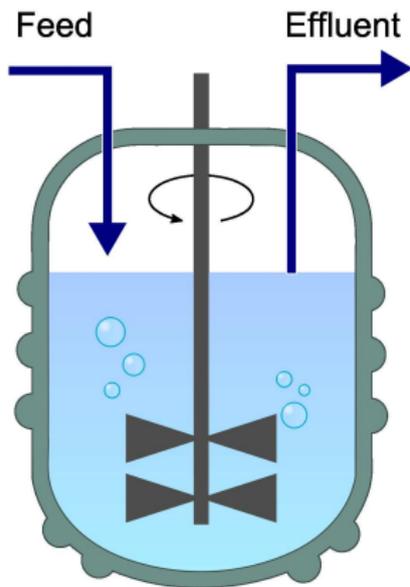
Published in *Automatica* in 2010

Sponsored by NSF/DMS Grant 0708084

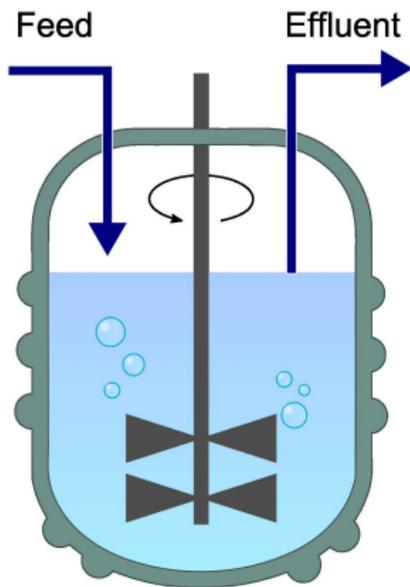
SIAM Minisymposium on Applications of Difference
and Differential Equations in Ecology and Epidemiology
2011 Joint Meetings, New Orleans

Chemostat Apparatus

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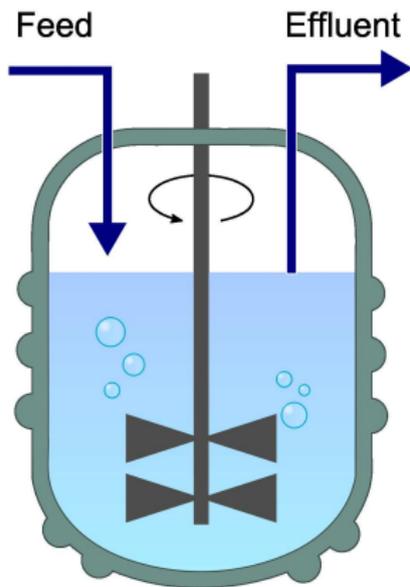


Chemostat Apparatus



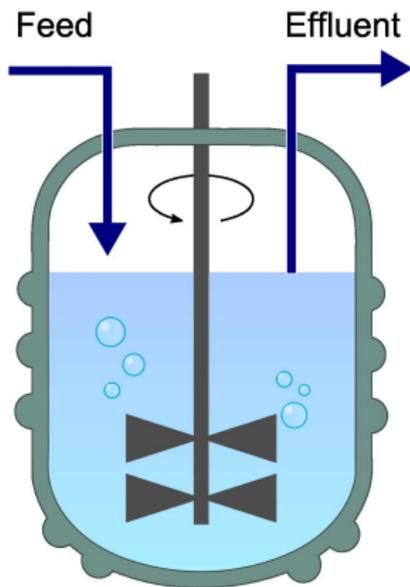
Bioreactor.

Chemostat Apparatus



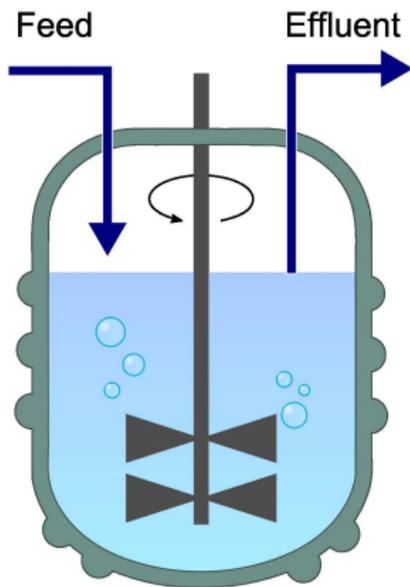
Bioreactor. Fresh medium continuously added.

Chemostat Apparatus



Bioreactor. Fresh medium continuously added. Culture liquid continuously removed.

Chemostat Apparatus



Bioreactor. Fresh medium continuously added. Culture liquid continuously removed. Culture volume constant.

Two-Species Chemostat Model

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- ▶ D cannot be constant if the μ_i 's are monotone.

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$$+ K_2 s_* x_{2*} \frac{L_2 g_1 - L_1 g_2}{\delta_2} > 0$$

$$\mathcal{U} = \frac{s_*}{(1-a)\mu_1(s_*)} \left[-K_1 + \frac{L_1 - g_1 s_*^2}{L_2 - g_2 s_*^2} K_2 \right] \neq 0 \quad (\text{SC})$$

- ▶ $\min\{\mu_1(s_{in}), \mu_2(s_{in})\} > \mu_1(s_*)$, and $L_2 g_1 - L_1 g_2 \leq 0$.
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Assumptions for Case where $G_1 > G_2$

- ▶ There is a constant $s_* \in (0, s_{in})$ such that $\mu_1(s_*) = \mu_2(s_*)$.
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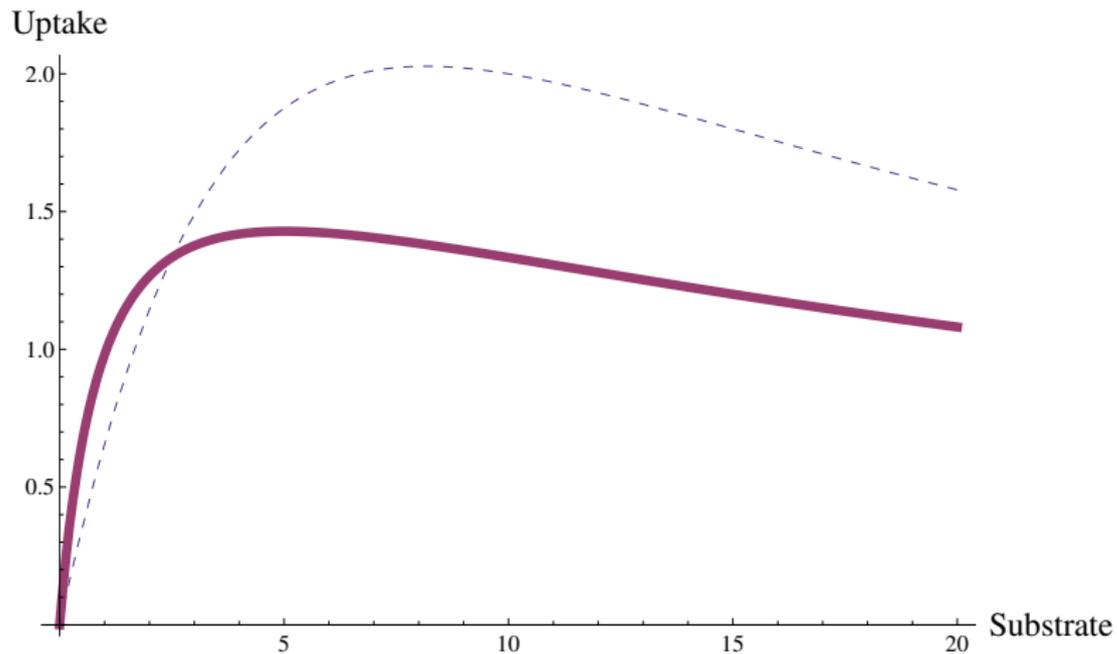
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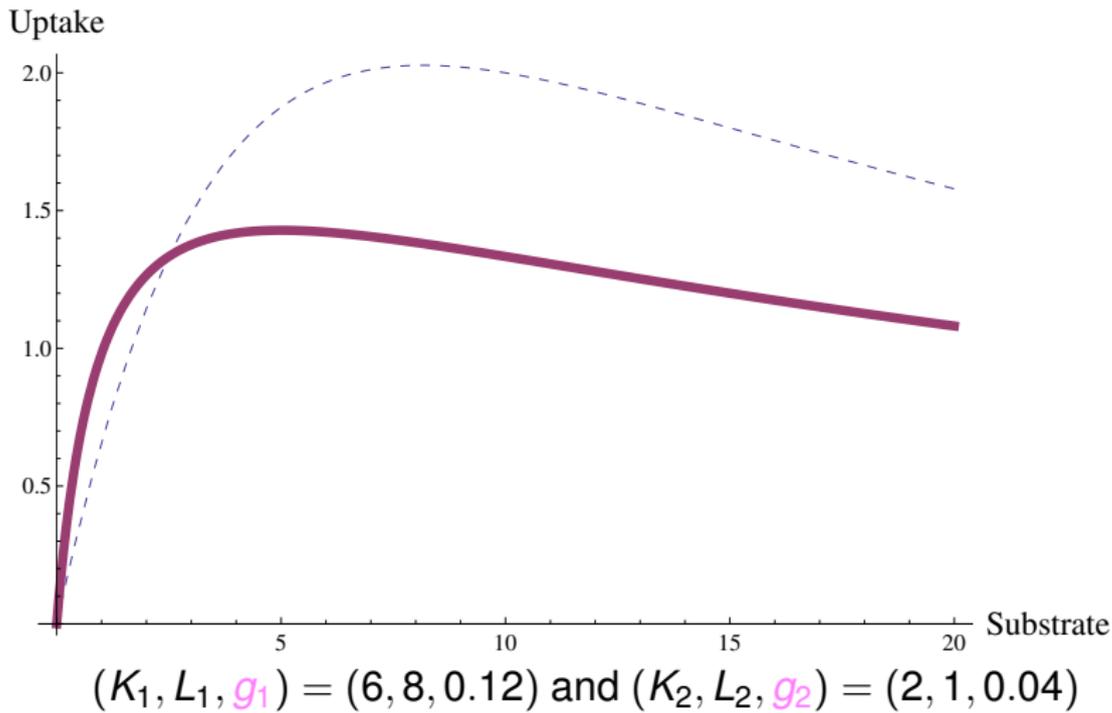
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$x_{1*}, x_{2*} > 0$ are any constants such that $s_* + x_{1*} + x_{2*} = s_{in}$.

Haldane Growth Functions



Haldane Growth Functions



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We can compute constants $\bar{\varepsilon}_i$ depending on τ_M so that for any constants $\varepsilon_i \in (0, \bar{\varepsilon}_i)$ for $i = 1, 2$ such that $\varepsilon_1 \varepsilon_2 \leq \bar{\varepsilon}_3$, the control

$$D = \mu_1(\mathbf{s}_*) - \text{sign}(\bar{U}) \varepsilon_1 \sigma(\varepsilon_2 \{x_1(t-\tau) + ax_2(t-\tau) - x_{1*} - ax_{2*}\})$$

globally asymptotically stabilizes $(\mathbf{s}_*, x_{1*}, x_{2*})$ for all initializations $(\phi_s, \phi_{x_1}, \phi_{x_2}) \in C([-2\tau_M, 0], (0, \infty)^3)$.

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$$\dot{U}_1 \leq -(\tilde{s} + \tilde{x}_1 + \tilde{x}_2)^2 - \frac{\kappa}{5} \frac{\tilde{s}^2}{s} - \frac{\varepsilon_1 \varepsilon_2 |\bar{U}|}{8} (\tilde{x}_1 + a\tilde{x}_2)^2, \quad t \geq \tau.$$

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The case $a = 1$ would give a nonisolated equilibrium.

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Corollary: We can choose K and a constant $\varepsilon > 0$ such that if $\mathcal{T}(\mu, \nu) = \max\{|\mu_i'(s) - \nu_i'(s)| : i = 1, 2; s \in [0, s_{in}]\} < \varepsilon$, then

$$\begin{cases} \dot{s} = D(y)[s_{in} - s] - \nu_1(s)x_1 - \nu_2(s)x_2 \\ \dot{x}_i = [\nu_i(s) - D(y)]x_i, \quad i = 1, 2 \end{cases} \quad (\text{RC})$$

is GAS to some point $(s_v, x_{1v}, x_{2v}) \in (0, \infty)^3$.

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- ▶ When $G_1 < G_2$, we can allow uncertain monotone uptake functions μ_j that are not necessary concave.
- ▶ When $G_1 > G_2$, we can cover time delays, nonmonotone uptake functions, and robustness to actuator errors.

Conclusions

- ▶ We achieved **output feedback GAS** of componentwise positive equilibria using only the sum of the species levels.
- ▶ Competitive exclusion required us to use a nonconstant controller to get permanence of both species.
- ▶ We dropped the usual assumption on the relative sizes of the growth yields G_j .
- ▶ When $G_1 < G_2$, we can allow uncertain monotone uptake functions μ_j that are not necessary concave.
- ▶ When $G_1 > G_2$, we can cover time delays, nonmonotone uptake functions, and robustness to actuator errors.
- ▶ Desirable extensions would allow more than two species, or multiple limiting substrates.